

Liquid Densities of γ -Butyrolactone and *N*-Methyl-2-pyrrolidone from 273 to 473 K and at Pressures up to 40 MPa

E. Christian Ihmels and Jürgen Gmehling*

Carl von Ossietzky University of Oldenburg, Department of Industrial Chemistry, P.O. Box 2503, D-26111 Oldenburg, Germany

Densities of γ -butyrolactone and *N*-methyl-2-pyrrolidone (NMP) have been measured with a computer-controlled high-temperature, high-pressure vibrating tube densimeter system (DMA-HDT) in the liquid state. The uncertainty in density measurement was estimated to be less than $\pm 0.2 \text{ kg}\cdot\text{m}^{-3}$ in the liquid state. The densities were measured for temperatures from 273 K to 473 K and pressures from 0.3 MPa up to 40 MPa, whereby a density range between (947 and 1168) $\text{kg}\cdot\text{m}^{-3}$ for γ -butyrolactone (353 data points) and between (865 and 1068) $\text{kg}\cdot\text{m}^{-3}$ for NMP (370 data points) was covered. The experimental data were correlated with the three-dimensional density correlation system (TRIDEN) and compared with published data.

Introduction

The main use of γ -butyrolactone is as an intermediate in the synthesis of *N*-methyl-2-pyrrolidone (NMP), pyrrolidone, herbicides, growth regulators, α -acetobutyrolactone (a vitamin B₁ intermediate), and the rubber additive thiodibutyric acid. Furthermore, γ -butyrolactone is used as a solvent for polymers, as a polymerization catalyst, in hair wave compositions, in suntan lotions, and in pharmaceuticals. It is also used in printing inks, for example, for ink-jet printing, as an extractant in the petroleum industry, as a stabilizer for chlorohydrocarbons and phosphorus-based pesticides, and as a nematocide.

Large-scale production of NMP is predominantly carried out by reacting γ -butyrolactone with methylamine. Because of its low volatility, thermal stability, high polarity, and aprotic, noncorrosive properties, NMP is an important solvent. Its auspicious toxicological and ecological properties account for the fact that NMP is replacing other solvents such as chlorinated hydrocarbons. NMP is used in many industrial fields, for example, for extraction of aromatics in petrochemical processing, for removal of CO₂ and H₂S in gas purifications, as an entrainer for extractive distillation processes, as a reaction medium for the production of polymers, and as a cleaning agent for silicon wafers.

Compressed liquid densities of NMP and γ -butyrolactone were measured with a computer-controlled vibrating tube densimeter. The densimeter had been calibrated with degassed water and butane and vacuum measurements. Densities were measured for temperatures from 273 K to 473 K and pressures from 0.3 MPa up to 40 MPa, whereby a density range between (947 and 1168) $\text{kg}\cdot\text{m}^{-3}$ for γ -butyrolactone (353 data points) and between (865 and 1068) $\text{kg}\cdot\text{m}^{-3}$ for NMP (370 data points) was covered. The measured densities of NMP and γ -butyrolactone were correlated with the three-dimensional correlating model TRIDEN. Details of the measurement system, the calibra-

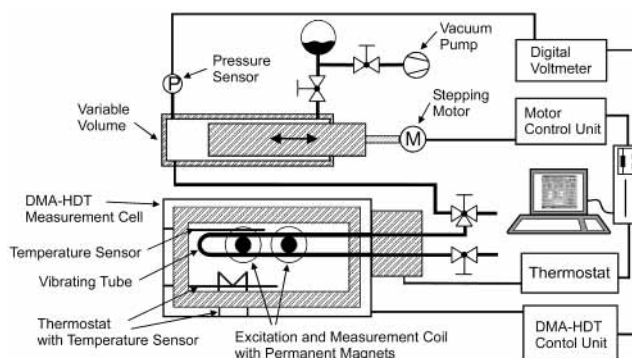


Figure 1. Schematic diagram of the computer-controlled density measurement unit.

tion, and the correlation are described by Ihmels and Gmehling.^{1,2}

Experimental Section

γ -Butyrolactone ($\text{C}_4\text{H}_6\text{O}_2$, $M = 86.09 \text{ g}\cdot\text{mol}^{-1}$, CAS-RN 96-48-0) and *N*-methylpyrrolidone (NMP, $\text{C}_5\text{H}_9\text{NO}$, $M = 99.13 \text{ g}\cdot\text{mol}^{-1}$, CAS-RN 872-50-4) were obtained from Acros and Riedel-de Haën, respectively. Both components were stored over a 3 Å molecular sieve and degassed by distillation. The final purities were checked by gas chromatography (γ -butyrolactone, >99.9 mass %; NMP, >99.98 mass %) and by Karl Fischer titration (water content of NMP < 20 ppm).

A computer-operated vibrating tube densimeter system for high temperatures and pressures (for temperatures from 273 to 623 K and pressures up to 40 MPa) was used for the measurement of the density data for γ -butyrolactone and NMP. The automated equipment can be used for the determination of densities in the sub- and supercritical states. With this apparatus, a large number of data points can be obtained in a rather short time with a minimum of manual effort. A temperature and pressure program can be driven to obtain a complete $P\rho T$ surface for the desired

* To whom correspondence should be addressed. E-mail: gmehling@tech.chem.uni-oldenburg.de. Telephone: ++49-441-798-3831. Fax: ++49-441-798-3330.

Table 1 (Continued)

<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³	<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³	<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³	<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³
443.12	34.994	1013.74	453.12	19.976	990.31	463.12	0.416	957.71	468.12	19.964	975.92
448.12	0.367	973.73	453.12	24.978	995.30	463.12	4.988	963.55	468.12	24.976	981.28
448.12	4.981	979.13	453.12	30.002	1000.18	463.12	9.957	969.54	468.11	29.977	986.44
448.12	9.996	984.71	453.12	34.986	1004.80	463.12	14.994	975.30	468.12	34.980	991.39
448.12	15.002	990.02	458.12	0.409	963.10	463.12	20.003	980.77	473.12	0.415	946.83
448.12	19.980	995.08	458.12	4.974	968.75	463.12	24.978	985.96	473.12	4.985	953.01
448.12	25.010	999.97	458.12	9.959	974.61	463.12	29.955	990.97	473.12	9.982	959.38
448.12	29.989	1004.72	458.12	14.976	980.20	463.12	34.990	995.87	473.11	14.991	965.42
448.12	34.996	1009.28	458.12	19.967	985.52	468.12	0.428	952.30	473.11	19.974	971.12
453.12	0.382	968.42	458.12	25.003	990.62	468.12	5.004	958.31	473.12	24.976	976.59
453.12	4.976	973.95	458.12	30.003	995.58	468.12	10.014	964.52	473.12	30.002	981.86
453.12	9.981	979.67	458.12	34.956	1000.35	468.12	14.979	970.35	473.12	34.992	986.92
453.12	14.960	985.09									

component. The measurement system was developed in the thesis of Ihmels.³ Densities as a function of temperature and pressure of several liquids and liquefied gases (e.g., toluene, carbon dioxide, carbonyl sulfide, hydrogen sulfide, sulfur hexafluoride, dinitrogen monoxide, R227ea, sulfur dioxide, MTBE, ETBE, DIPE, 1-butanol, and DIPE/1-butanol mixtures) have already been published.¹⁻⁷ The comparisons with reference equations of state (EoS) for toluene, CO₂, and SF₆ demonstrated the high accuracy and suitability of this measurement system. Using the measured densities of sulfur dioxide, a new Helmholtz-type equation of state was developed by Ihmels et al.⁷

The apparatus and procedure of the measurements are described in detail by Ihmels and Gmehling.^{1,2} A scheme of the density measurement system is shown in Figure 1. A prototype of a high-pressure, high-temperature vibrating tube densimeter (DMA-HDT) from "Labor für Meßtechnik Dr. Hans Stabinger" (Graz, Austria) is the essential part of the experimental setup. The temperature is measured using a Pt100 resistance thermometer, and the pressure is monitored by means of a calibrated external pressure sensor (model PDCR 911, pressure range 60 MPa, Druck). The density values are obtained from the periods of oscillation of the vibrating tube. For the calibration, the period of oscillation at zero pressure and the two reference substances water and butane were used. The reference densities were calculated using the reference EoS from Wagner and Pruss^{8,9} for water and the EoS from Younglove and Ely¹⁰ for butane. The uncertainty of the temperature is estimated to be ± 0.03 K, and the pressure has an estimated uncertainty of ± 6 kPa. For density measurements in the temperature and pressure ranges covered (273 K to 473 K, 0.3 MPa to 40 MPa) a maximum error of ± 0.2 kg·m⁻³ is obtained.

Results and Discussion

In this work, the densities of γ -butyrolactone (353 data points) and NMP (370 data points) in the compressed liquid state were measured from 273 K to 473 K and from 0.3 MPa up to 40 MPa. The results are listed in Tables 1 and 2 and presented graphically in Figures 2 and 3.

Aside from several published¹¹ density measurements at atmospheric or saturation pressure for γ -butyrolactone up to 553 K and NMP up to 373 K, compressed liquid densities were measured only for γ -butyrolactone at 293 K and up to 10 MPa by Fornefeld-Schwarz et al.¹² Therefore, these new measurements represent a wide extension of the $P\rho T$ data for γ -butyrolactone and NMP.

The measured densities were correlated with the three-dimensional $P\rho T$ -correlating model TRIDEN.¹⁻³ In this

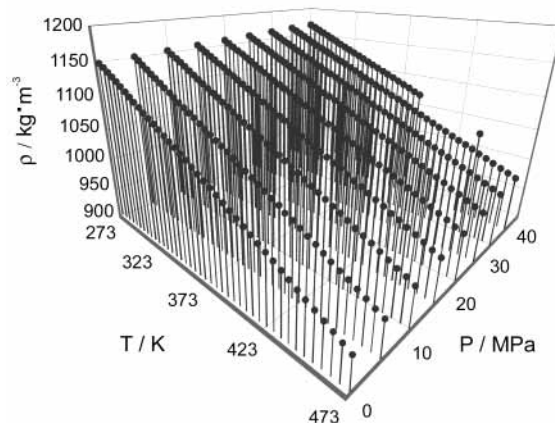


Figure 2. Densities of γ -butyrolactone at temperatures between 273 K and 473 K and pressures between 0.3 and 40 MPa.

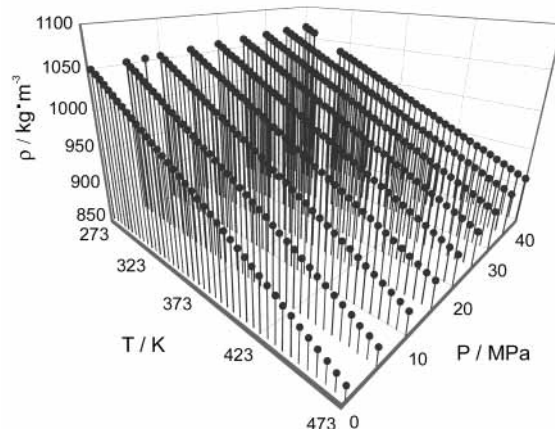


Figure 3. Densities of NMP at temperatures between 273 K and 473 K and pressures between 0.3 and 40 MPa.

model the Tait equation for isothermal compressed densities was combined with a modified Rackett equation for the liquid saturation densities and the Wagner vapor pressure equation in the "2.5,5" form, used as a reference state (ρ_0 and P_0), which is required for the Tait equation. Using these equations, it is possible to correlate the $P\rho T$ data in the whole liquid state up to the critical point, nearly within experimental error. The TRIDEN model is also applicable for correlations of mixture densities and the calculation of excess volumes.⁶ In this work only densities up to the vicinity of the normal boiling points were measured. Therefore, the Wagner vapor pressure equation was omitted and 0.1013 MPa was used as a fixed reference pressure for all temperatures. The reference densities ρ_0 at $P_0 = 0.1013$ MPa were extrapolated from the compressed

Table 2 (Continued)

<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³	<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³	<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³	<i>T</i> /K	<i>P</i> /MPa	ρ /kg·m ⁻³
438.09	30.004	928.54	448.09	25.004	915.85	458.09	19.989	902.49	468.09	10.022	882.56
438.09	35.004	932.72	448.09	29.993	920.38	458.09	24.979	907.46	468.08	14.961	888.32
438.09	40.005	936.75	448.09	34.986	924.74	458.09	30.022	912.26	468.09	19.989	893.86
443.09	0.392	894.74	448.09	40.015	928.97	458.09	35.006	916.79	468.09	25.028	899.13
443.09	5.006	899.98	453.09	0.393	885.03	458.09	39.998	921.12	468.08	29.966	904.05
443.09	9.985	905.38	453.09	5.028	890.63	463.09	0.416	875.19	468.09	35.003	908.83
443.09	15.012	910.52	453.09	9.984	896.29	463.09	4.954	881.04	468.08	39.969	913.34
443.09	19.977	915.35	453.09	15.028	901.72	463.09	10.005	887.11	473.08	0.431	865.24
443.09	24.982	920.00	453.09	20.025	906.83	463.09	14.984	892.80	473.08	4.995	871.49
443.09	30.008	924.48	453.09	24.958	911.62	463.09	19.985	898.17	473.08	9.982	877.88
443.09	35.018	928.75	453.09	30.022	916.33	463.09	24.969	903.26	473.08	15.006	883.90
443.09	39.986	932.83	453.09	34.965	920.74	463.09	29.990	908.15	473.08	19.980	889.52
448.09	0.360	889.86	453.09	39.978	925.02	463.09	35.028	912.83	473.08	24.975	894.87
448.09	5.009	895.32	458.09	0.406	880.13	463.09	39.978	917.24	473.08	29.975	899.96
448.09	9.959	900.81	458.09	5.033	885.88	468.09	0.423	870.23	473.08	34.999	904.84
448.09	14.962	906.07	458.09	10.016	891.75	468.08	5.017	876.34	473.08	40.018	909.50
448.09	20.008	911.10	458.09	14.959	897.21						

liquid density measurements and correlated with the modified Rackett eq 1:

$$\rho_0 = A_R/B_R^{[1+(1-T/C_R)^{D_R}]} \quad (1)$$

For the Tait equation (eq 2)

$$\rho = \rho_0 \left[1 - C_T \ln \left(\frac{B_T + P}{B_T + P_0} \right) \right] \quad (2)$$

the following temperature dependence is used for the parameter B_T :

$$B_T = b_0 + b_1 \frac{T}{E_T} + b_2 \left(\frac{T}{E_T} \right)^2 + b_3 \left(\frac{T}{E_T} \right)^3$$

The parameter C_T is a temperature independent constant.

Along with a deviation plot, other statistical values are desirable to evaluate the correlation. The absolute (RMSD) and relative (RMSDr) root-mean-square deviations and the mean deviation (bias) are used as statistical values for the TRIDEN fits.

$$\text{RMSD} = \sqrt{\frac{1}{n} \sum (\rho_{\text{exp}} - \rho_{\text{calc}})^2} \quad (3)$$

$$\text{RMSDr} = 100 \sqrt{\frac{1}{n} \sum \left(\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\rho_{\text{exp}}} \right)^2} \quad (4)$$

$$\text{bias} = \frac{1}{n} \sum (\rho_{\text{exp}} - \rho_{\text{calc}}) \quad (5)$$

The TRIDEN parameters for the Tait equation, parameters for the Rackett equation, the temperature and pressure ranges covered, and additional statistical values are given in Table 3. The units are K, MPa, and kg·m⁻³.

In Figures 4 and 5 the relative deviations between experimental values and the correlation are shown. The deviations are usually within $\pm 0.04\%$ except at some points at the extremes of temperatures.

The deviations between the TRIDEN correlation for γ -butyrolactone and the densities of Fornefeld-Schwarz et al.¹² at 293 K are -0.04% at all pressures (up to 10 MPa). A comparison was also made between the DDB-Pure¹¹ correlations of experimental saturated liquid densities from different researchers and the TRIDEN correlations. The very good relative root-mean-square deviations of 0.22%

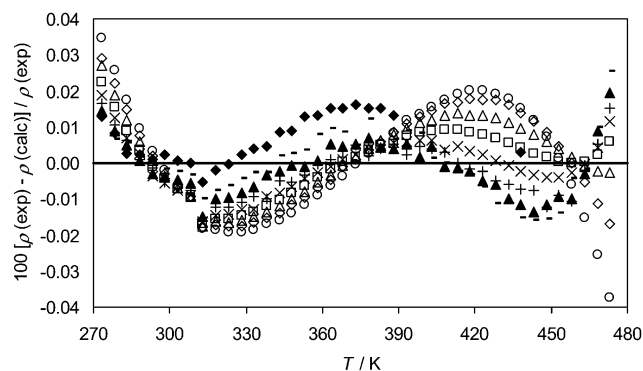


Figure 4. Relative deviations between experimental densities and the TRIDEN correlation for γ -butyrolactone: \circ , < 5 MPa; \diamond , 5 MPa; \triangle , 10 MPa; \square , 15 MPa; \times , 20 MPa; $+$, 25 MPa; \blacktriangle , 30 MPa; $-$, 35 MPa; \blacklozenge , 40 MPa.

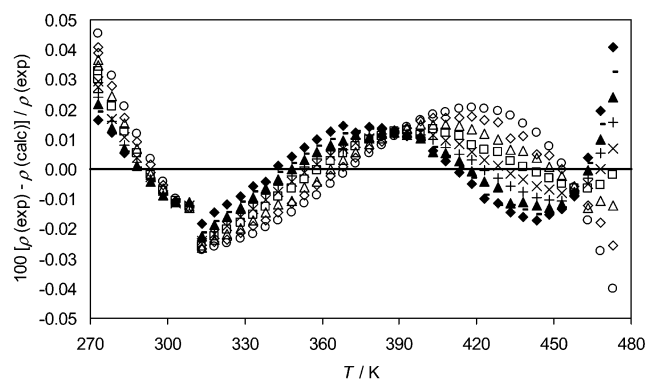


Figure 5. Relative deviations between experimental densities and the TRIDEN correlation for NMP: \circ , < 5 MPa; \diamond , 5 MPa; \triangle , 10 MPa; \square , 15 MPa; \times , 20 MPa; $+$, 25 MPa; \blacktriangle , 30 MPa; $-$, 35 MPa; \blacklozenge , 40 MPa.

for γ -butyrolactone (from 273 K to 473 K) and 0.07% for NMP (from 273 K to 373 K) are a further indication of the good quality of the measurements and the correlation.

Summary

Densities in the compressed liquid state were presented for γ -butyrolactone and *N*-methyl-2-pyrrolidone (NMP) for temperatures between 273 K and 473 K and pressures up to 40 MPa. These measurements represent a wide extension of the $P\rho T$ data for γ -butyrolactone and NMP. All data were correlated with the TRIDEN model and show very good agreement with other published densities.

Table 3. Parameters for the TRIDEN Correlation Model for γ -Butyrolactone and NMP: Temperature Range, Pressure Range, Number of Data Points, Tait Parameters, and Rackett Parameters, and Absolute (RMSD) and Relative (RMSDr) Root-Mean-Square Deviations and the Mean Deviation (bias) as Statistical Values for the TRIDEN Fit

	γ -butyrolactone	NMP
T_{\min}/K	273.2	273.2
T_{\max}/K	473.1	473.1
P_{\min}/MPa	0.26	0.26
P_{\max}/MPa	40	40
$\rho_{\min}/\text{kg}\cdot\text{m}^{-3}$	946.8	865.2
$\rho_{\max}/\text{kg}\cdot\text{m}^{-3}$	1167.7	1067.7
no. of data points	353	370
c_0	0.101 086	0.089 074
b_0/MPa	446.139	322.577
b_1/MPa	-34.4609	10.1783
b_2/MPa	-27.5124	-33.1819
b_3/MPa	3.810 49	4.033 94
E_r/K	100	100
$A_R/\text{kg}\cdot\text{m}^{-3}$	27.7137	29.4842
B_R	0.140 804	0.1520 53
C_R/K	851.568	837.678
D_R	0.273 244	0.277 313
RMSD/ $\text{kg}\cdot\text{m}^{-3}$	0.1120	0.1377
RMSDr/%	0.0105	0.0139
bias/ $\text{kg}\cdot\text{m}^{-3}$	-0.000 76	0.001 59

The density measurements for γ -butyrolactone and NMP are a continuation of the density measurements performed for toluene, carbon dioxide, carbonyl sulfide, hydrogen sulfide, sulfur hexafluoride, dinitrogen monoxide, R227ea, sulfur dioxide, some ethers (MTPE, ETBE, and DIPE), and mixtures (DIPE/1-butanol).¹⁻⁷

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